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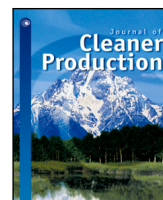
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Maximizing thermal efficiency of a cavity using hybrid nanofluid

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ABSTRACT

Background: Increasing population growth and economic progress are partially to blame for the global issue of climate change and rising energy usage. One important step towards dealing with this issue would be to enhance the efficiency of a thermal system using tiny nanoparticles. Adding hybrid nanoparticles in a working fluid results in a “hybrid nanofluid” which can improve the efficiency of a thermal system to meet the rising demand for energy for current technology.

Aim: This study aims to increase the heat transfer in an inclined cavity using Ag–TiO₂ nanoparticles. The novel aspects of this research include evaluating the thermal performance of the suggested thermal system in the presence of a magnetic field and thermal radiation. Moreover, the heat transfer ability of a regular fluid, nanofluid, and hybrid nanofluid will also be compared with each other.

Methodology: The finite difference method is used to obtain the numerical solutions. The computations are done using MATLAB software.

Findings: The findings show that the applied magnetic field boosts the heat transfer capacity of nanoparticles. The heat transfer of the fluid increased by 1.6% and 2.5% on adding 4% vol. of TiO₂ and Ag–TiO₂ nanoparticles, respectively.

1. Introduction

Climate change and the increasing energy consumption in the world have become a worldwide issue, growing populations, and economic advancement are somehow responsible for this. Nano-materials may overcome these barriers due to their properties and nanoscale size (Hamzat et al., 2022; Hanif et al., 2024; Bratovic, 2019; Hanif and Shafie, 2022c). However, these newly developing nanomaterials should have minimal operating costs because they will be used in areas with little infrastructure. Titanium oxide (TiO₂) is an ideal material in this context because it is photo-catalytically active, stable (in both acidic and basic environments), readily available, and nontoxic (Sanzone et al., 2018; Hovazi and Rostami, 2023; Hanif et al., 2023b). It is frequently utilized as a less expensive substitute for the standard industrial transparent conducting oxides. The primary concern with using titanium dioxide is its poor efficiency. Only 7% of solar energy can be used due to its broadband gap (3.2 eV), which results in low efficiency for solar-powered applications. Several alternative tactics have been attempted to maximize the efficiency of titanium dioxide consumption, one of which is combining TiO₂ with tiny silver Ag nanoparticles. Chakhtouna et al. (2021) discussed the significance of silver (Ag) nanoparticles in raising the Ag/TiO₂ photocatalysts'

antibacterial activities. Transparent conducting oxide thin films are widely utilized in industry for a wide range of applications, including electrochromic devices and solar cells. In this regard, Dhar and Alford (2013) deposited the superior transparent TiO₂–Ag–TiO₂ composite electrode films by sputtering at ambient temperature on a substrate. Yu et al. (2011) claimed that the bactericidal activities of the synthesized Ag–TiO₂ thin films were higher than those of the plain TiO₂ nanofilm. Clinics and industries can use TiO₂ and Ag-deposited nanotubes for antibacterial purposes, especially because of their reusable nature (Li et al., 2013). Several authors discussed how the performance of TiO₂ can be enhanced by combining it with Ag nanoparticles (Hanif et al., 2023a; Chawhan et al., 2021; Soylu et al., 2022; Li et al., 2020). Keeping these environmentally friendly use of Ag and TiO₂ nanoparticles, this research is designed to analyze the significance of Ag–TiO₂ nanoparticles on the thermal efficiency of an energy-intensive system.

The wide range of engineering applications for convective heat transfer in thermal cavities, including heat exchangers, cooling electronics, fuel cells, geothermal power plants, food processing, and solar thermal systems, have made them highly sought-after. The mass–energy interaction between the surrounding and the moving fluid within a rectangular enclosure is known as convective heat transfer in a cavity.

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Nomenclature**Roman letters**

(u, v)	Velocity components
B_0	Magnetic field strength
C_p	Specific heat capacity
g	Gravitational acceleration
k	Thermal conductivity
k_b	Absorption parameter
Nu	Nusselt number
T	Temperature
t	Time
Ec	Eckert number
M	Magnetic parameter
Pr	Prandtl number
Ra	Rayleigh number
Rd	Radiation parameter

Greek letters

β_T	Volumetric thermal expansion
$\chi_1 - \chi_6$	Nanofluid constants
Δt	Time step
Δx	Grid size in x direction
Δy	Grid size in y direction
μ	Dynamic viscosity
ν	Kinematic viscosity
ω	Vorticity
ψ	Stream function
ρ	Density
σ	Electrical conductivity
σ_b	Stefan Boltzman parameter
φ	Nanoparticles volume fraction

Subscripts/Superscripts

(p_1, p_2)	Nanoparticles
*	Non-dimensional
f	Base fluid
hnf	Hybrid nanofluid
i	Grid point in x direction
j	Grid point in y direction
k	Time level
nf	Nanofluid

This interaction might be forced, mixed, or natural convection, depending on how the buoyancy and external forces are distributed (Hussien et al., 2021). The major efforts have been directed at improving the cavities' heat transport to fulfill the growing demand for engineering applications. Reddy et al. (2022) examined the behavior of multiwall carbon nanotubes (MWCNTs) in the fluid that was flowing in a square cavity with magnetic effects and detected that a 4% volume fraction of MWCNTs can improve the heat transfer rate by 7.2%. Turkyilmazoglu (2022a) investigated the fluid flow in a lid-driven cavity with a single lid divided into two distinct joint walls representing possible stirrers. Later, he extended his work to heat transfer analysis of the fluid flow inside a square cavity with a centrally located nonuniform heating wall (Turkyilmazoglu, 2022b). It was noticed that the heat transmission improved when an unevenly heated wall extended from the bottom to the top of the wall. The consequences

of ternary nanoparticles (Fe_3O_4 -MWCNTs-Cu) on the thermal performance of a cavity are investigated by Thirumalaisamy and Reddy (2023). They observed that the heat transfer rate increased by 3.4% on considering the Fe_3O_4 -MWCNTs-Cu with the ratio 25:50:25 instead of 25:25:50. Selimefendigil and Chamkha (2021) analyzed the heat transfer characteristics of a square cavity containing a triangular-shaped segmented porous surface in the presence of Ag and MgO nanoparticles. They found that the average Nusselt number increased by 14.7% with 1% vol. fraction of Ag nanoparticles and 6.89% with 1% vol. fraction of MgO nanoparticles. Some interesting discussions on the significance of hybrid nanofluid inside a thermal system can be found in Hanif et al. (2022b), Acharya (2021), Giwa et al. (2020), Hanif and Shafie (2022a), Scott et al. (2022).

The magnetohydrodynamic (MHD) principle is significantly important in power generation, energy harvesting, pumping of materials, space transportation, astrophysical environments, and biomedical (Hanif and Shafie, 2022b; Avalos-Zúñiga and Rivero, 2022; Seo and Ryu, 2023; Hanif et al., 2022a). The MHD system can potentially replace or supplement the traditional fossil fuel-based generating system, laying the groundwork for a completely sustainable society (Gupta et al., 2021). Many scientists have been interested in MHD fluid flow and heat transfer in a confined cavity considering the impact of natural convection due to its practical uses in cooling and heating applications (Mirzaei et al., 2023). The convective-radiative heat transfer of Al_2O_3 -CuO/ H_2O flow in the presence of magnetic field is considered by Atashafrooz et al. (2023). According to their results, the maximum heat transfer rates were obtained in the absence of magnetic force with 3% Al_2O_3 :3%CuO when radiative parameter ($Rd = 1$). Natural convection in MHD conjugate flow of a water-based nanofluid in an inclined cavity is discussed by Tasnim et al. (2023). The impact of nanoparticle shape on the natural convective heat transfer of a nanofluid in a wavy-walled cavity is investigated by Saha et al. (2023). According to their results, the heat transfer increased by 2.86% and 7.65% with spherical-shaped and blade-shaped nanoparticles, respectively. Tayebi and Chamkha (2020) investigated the consequences of the magnetic field on the irreversibility process in a square cavity using water-based Cu- Al_2O_3 hybrid nanofluid. Atashafrooz et al. (2020) discussed the interaction of magnetic field on heat transfer and entropy generation of CuO/ H_2O nanofluid flow in a trapezoidal recess. Atashafrooz (2020) analyzed the consequences of magnetic field and thermal radiation on the thermal behavior of CuO/ H_2O and Al_2O_3 / H_2O over an inclined step. Their findings indicate that the heat transfer rates are more impacted by CuO nanoparticles than by Al_2O_3 nanoparticles. Some good discussions on how a magnetic field affects the performance of a hybrid nanofluid in a cavity are given in Rashidi et al. (2021), Lawrence and Kumar (2021), Mansour et al. (2020), Roy (2022) and Sajjadi et al. (2018).

The aforementioned literature reveals that the convective heat transfer in thermal cavities is attracting the attention of researchers due to its broad applications in industry and science. Although several studies discussed heat transfer in thermal cavities, most of these studies considered steady cases where the time factor was ignored. However, some studies discussed the time-dependent convective heat transfer in cavities but those studies considered either regular fluid or mono nanofluids as a working fluid. It is important to mention that the desired heat transfer rates cannot be achieved using regular fluids due to their low thermal conductivity. The issue with mono nanofluids is that they either have high thermal efficiency or excellent physico-chemical properties. A mono nanofluid does not have all of the needed properties for certain applications. To fill this research gap, the primary aim of this study is to examine an unsteady convective heat transfer in a square cavity and analyze how Ag-TiO₂/water hybrid nanofluid improves the thermal efficiency of a system. Furthermore, the addition of nanoparticles to the base fluid and the application of an external magnetic field can serve as both passive and active control mechanisms by regulating heat transmission in a thermal system (Geridonmez and

Table 1
Thermo-physical properties of nanoparticles and base fluid (Hanif et al., 2023a).

Material	ρ kg/m ³	β 1/K	C_p J/kgK	k W/mK	σ S/m
Ag	10 500	1.89×10^{-5}	235	429	6.3×10^7
TiO ₂	4250	0.9×10^{-5}	686.2	8.9538	2.6×10^6
H ₂ O	997.1	21×10^{-5}	4179	0.613	5.5×10^{-6}

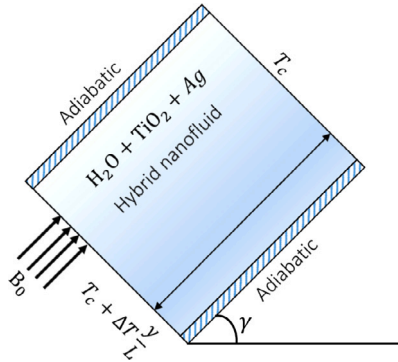


Fig. 1. Graphical representation.

Oztop, 2020). Therefore, this study also examines the impact of an external magnetic field on the thermal performance of the hybrid nanofluid in the presence of thermal radiation, which has not been studied before. The mathematical model comprised of the 2D coupled partial differential equations. A finite difference numerical technique is used to tackle the numerical solutions of the problem. It is important to note that solving the Navier–Stokes equations is a challenging task, and an analytical solution is not always available. Therefore, numerical approaches such as the finite difference method can be used to estimate the numerical solutions. The obtained numerical results are presented with the help of figures and tables.

2. Properties of Ag, TiO₂, and H₂O

Every material either fluid or solid has its own thermal properties; heat capacity, thermal expansion, and thermal conductivity; physical properties such as dynamic viscosity, density, and electrical conductivity. Table 1 illustrates these properties of silver (Ag), titanium oxide (TiO₂) and water (H₂O).

3. Physical model

The natural convection of an incompressible hybrid nanofluid flow in an inclined square cavity with Rosseland heat flux is investigated in this work. The cavity is bounded by two adiabatic (horizontal) and two isothermal (vertical) walls. The left wall of the cavity is continuously heated with the temperature $T_c + \Delta T(y/L)$, while the right wall is kept at a constant temperature of T_c . Hybrid nanoparticles Ag–TiO₂ are added to the working fluid and a magnetic field is applied uniformly to the vertical axis. Moreover, the effects of Joule heating are also taken into account. Fig. 1 depicts the graphical representation of the mathematical model.

4. Mathematical model

The considered physical model is governed by the law of conservation of mass, momentum, and energy (Tasnim et al., 2023):

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

$$\rho_{hnf} \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial x} + \mu_{hnf} \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) + g(\rho\beta_T)_{hnf} (T - T_c) \sin \gamma, \tag{2}$$

$$\rho_{hnf} \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = - \frac{\partial p}{\partial y} + \mu_{hnf} \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) - \sigma_{hnf} B_0^2 v + g(\rho\beta_T)_{hnf} (T - T_c) \cos \gamma, \tag{3}$$

$$(\rho C_p)_{hnf} \left(\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = k_{hnf} \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) - \left(\frac{\partial q_{rx}}{\partial x} + \frac{\partial q_{ry}}{\partial y} \right) + \sigma_{hnf} B_0^2 v^2. \tag{4}$$

Initially, the fluid was at rest with wall temperature T_c , therefore, at $t \leq 0$:

$$u = 0; v = 0; T = T_c. \tag{5}$$

The prescribed boundary conditions at $t > 0$ are:

- all walls: $u = 0; v = 0$,
- horizontal walls: $\frac{\partial T}{\partial y} = 0$,
- left wall: $T = T_c + \Delta T \frac{y}{L}$,
- at right wall: $T = T_c$.

The Rosseland approximation for the heat fluxes q_{rx} and q_{ry} in the energy Eq. (4) are given as Sivasankaran et al. (2020):

$$\frac{\partial q_{rx}}{\partial x} = - \frac{16\sigma_b T_c^3}{3k_b} \frac{\partial^2 T}{\partial x^2}, \quad \text{and} \quad \frac{\partial q_{ry}}{\partial y} = - \frac{16\sigma_b T_c^3}{3k_b} \frac{\partial^2 T}{\partial y^2}. \tag{7}$$

The physical and thermal properties of hybrid nanofluid; density (ρ_{hnf}), dynamic viscosity (μ_{hnf}), thermal expansion ($(\rho\beta_T)_{hnf}$), electrical conductivity (σ_{hnf}), heat capacity ($(\rho C_p)_{hnf}$), and thermal conductivity (k_{hnf}) are presented as Hanif et al. (2023a):

$$\begin{aligned} \rho_{hnf} &= (1 - \varphi_{p_2})\rho_{nf} + \varphi_{p_2}\rho_{p_2}, \quad \rho_{nf} = (1 - \varphi_{p_1})\rho_f + \varphi_{p_1}\rho_{p_1}, \\ \mu_{hnf} &= \frac{\mu_f}{(1 - \varphi_{p_1})^{2.5} (1 - \varphi_{p_2})^{2.5}}, \\ \frac{\sigma_{hnf}}{\sigma_{nf}} &= \frac{(\sigma_{p_2} + 2\sigma_{nf}) + 2\varphi_{p_2}(\sigma_{p_2} - \sigma_{nf})}{(\sigma_{p_2} + 2\sigma_{nf}) - \varphi_{p_2}(\sigma_{p_2} - \sigma_{nf})}, \\ \frac{\sigma_{nf}}{\sigma_f} &= \frac{(\sigma_{p_1} + 2\sigma_f) + 2\varphi_{p_1}(\sigma_{p_1} - \sigma_f)}{(\sigma_{p_1} + 2\sigma_f) - \varphi_{p_1}(\sigma_{p_1} - \sigma_f)}, \\ (\rho\beta_T)_{hnf} &= (1 - \varphi_{p_2})(\rho\beta_T)_{nf} + \varphi_{p_2}(\rho\beta_T)_{p_2}, \\ (\rho\beta_T)_{nf} &= (1 - \varphi_{p_1})(\rho\beta_T)_f + \varphi_{p_1}(\rho\beta_T)_{p_1}, \\ (\rho C_p)_{hnf} &= (1 - \varphi_{p_2})(\rho C_p)_{nf} + \varphi_{p_2}(\rho C_p)_{p_2}, \\ (\rho C_p)_{nf} &= (1 - \varphi_{p_1})(\rho C_p)_f + \varphi_{p_1}(\rho C_p)_{p_1}, \\ \frac{k_{hnf}}{k_{nf}} &= \frac{(k_{p_2} + 2k_{nf}) + 2\varphi_{p_2}(k_{p_2} - k_{nf})}{(k_{p_2} + 2k_{nf}) - \varphi_{p_2}(k_{p_2} - k_{nf})}, \\ \frac{k_{nf}}{k_f} &= \frac{(k_{p_1} + 2k_f) + 2\varphi_{p_1}(k_{p_1} - k_f)}{(k_{p_1} + 2k_f) - \varphi_{p_1}(k_{p_1} - k_f)}. \end{aligned} \tag{8}$$

Let us consider the following non-dimensional variables (Geridonmez and Oztop, 2020):

$$\begin{aligned} x^* &= \frac{x}{L}, y^* = \frac{y}{L}, t^* = \frac{t\alpha_f}{L^2}, u^* = \frac{uL}{\alpha_f}, v^* = \frac{vL}{\alpha_f}, \\ T^* &= \frac{T - T_c}{\Delta T}, p^* = \frac{pL^2}{\rho_f \alpha_f^2}, \psi^* = \frac{\psi}{\alpha_f}, \omega^* = \frac{\omega L^2}{\alpha_f}, \alpha_f = \frac{k_f}{(\rho C_p)_f}. \end{aligned} \tag{9}$$

Before we proceed further, let us define the relationship of stream function (ψ) and the vorticity (ω) with the velocity (u, v):

$$u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x}, \quad \omega = \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y}. \tag{10}$$

Exploiting Eqs. (7)–(10) to the governing Eqs. (1)–(4) yields us to a set of non-dimensional equations (after removing ‘*’):

$$\frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} = -\omega, \tag{11}$$

$$\frac{\chi_1}{Pr} \left(\frac{\partial \omega}{\partial t} + u \frac{\partial \omega}{\partial x} + v \frac{\partial \omega}{\partial y} \right) = \chi_2 \left(\frac{\partial^2 \omega}{\partial x^2} + \frac{\partial^2 \omega}{\partial y^2} \right) - \chi_3 M \frac{\partial v}{\partial x} + \chi_4 Ra \left(\frac{\partial T}{\partial x} \cos \gamma - \frac{\partial T}{\partial y} \sin \gamma \right), \tag{12}$$

$$\chi_5 \left(\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = (\chi_6 + Rd) \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) + \frac{\chi_3 M Ec}{Pr} v^2. \tag{13}$$

Here χ_1 – χ_6 , M , Rd , Pr , Ec , and Ra are the non-dimensional parameters defined as

$$\begin{aligned} \chi_1 &= \frac{\rho_{hnf}}{\rho_f}, \quad \chi_2 = \frac{\mu_{hnf}}{\mu_f}, \quad \chi_3 = \frac{\sigma_{hnf}}{\sigma_f}, \quad \chi_4 = \frac{(\rho\beta_T)_{hnf}}{(\rho\beta_T)_f}, \\ \chi_5 &= \frac{(\rho C_p)_{hnf}}{(\rho C_p)_f}, \quad \chi_6 = \frac{k_{hnf}}{k_f}, \\ M &= \frac{\sigma_f B_0^2 L^2}{\mu_f}, \quad Rd = \frac{16\sigma_b T_c^3}{3k_b k_f}, \quad Pr = \frac{\nu_f}{\alpha_f}, \\ Ec &= \frac{v_f^2}{\Delta T (C_p)_f L^2}, \quad Ra = \frac{g(\beta_T)_f \Delta T L^3}{\nu_f \alpha_f}. \end{aligned} \tag{14}$$

The non-dimensional initial and boundary conditions are:

- all walls: $u = 0; v = 0; T = 0, \quad t \leq 0,$
- horizontal walls: $u = 0; v = 0, \quad \frac{\partial T}{\partial y} = 0, \quad t > 0,$
- left vertical wall: $u = 0; v = 0, \quad T = y, \quad t > 0,$
- right vertical wall: $u = 0; v = 0, \quad T = 0, \quad t > 0.$

The Nusselt number on the left wall can be defined as:

$$Nu = -\chi_6 \left(\frac{\partial T}{\partial x} \right)_{x=0}. \tag{16}$$

5. Numerical procedure

Let $\psi_{i,j}^k, \omega_{i,j}^k,$ and $T_{i,j}^k$ be the numerical solutions of stream function, vorticity, and temperature at (x_i, y_j, t_k) , respectively. Given that $t_k = k\Delta t, k = 0, 1, \dots, m, x_i = i\Delta x, i = 1, 2, \dots, p, y_j = j\Delta y, j = 1, 2, \dots, q,$ where $\Delta t = t_f/m$ is the time step, $\Delta x = x_{max}/p$ is the mesh size along x -axis and $\Delta y = y_{max}/q$ is the mesh size along y -axis. Let f be any general continuous function and $f_{i,j}^k$ be the numerical solution at (x_i, y_j, t_k) then the forward difference for the time derivative and the central difference for the spatial derivatives are given as (Hanif, 2021a,b, 2022):

- time derivative

$$\frac{\partial f}{\partial t}(x_i, y_j, t_k) \approx \frac{f_{i,j}^{k+1} - f_{i,j}^k}{\Delta t}. \tag{17}$$

- spatial first-order derivatives

$$\frac{\partial f}{\partial x}(x_i, y_j, t_k) \approx \frac{f_{i+1,j}^k - f_{i-1,j}^k}{2\Delta x}, \quad \text{and} \quad \frac{\partial f}{\partial y}(x_i, y_j, t_k) \approx \frac{f_{i,j+1}^k - f_{i,j-1}^k}{2\Delta y}. \tag{18}$$

- spatial second-order derivatives

$$\begin{aligned} \frac{\partial^2 f}{\partial x^2}(x_i, y_j, t_k) &\approx \frac{f_{i+1,j}^k - 2f_{i,j}^k + f_{i-1,j}^k}{\Delta x^2}, \quad \text{and} \\ \frac{\partial^2 f}{\partial y^2}(x_i, y_j, t_k) &\approx \frac{f_{i,j+1}^k - 2f_{i,j}^k + f_{i,j-1}^k}{\Delta y^2}. \end{aligned} \tag{19}$$

Using the aforementioned time and spatial derivatives in Eqs. (11)–(13) and rearranging the resultant equations lead us to:

$$\psi_{i,j}^{k+1} \approx \omega_{i,j}^k + \mathcal{L}_{i,j}^{k+1}[\psi] + \mathcal{U}_{i,j}^k[\psi]. \tag{20}$$

$$\omega_{i,j}^{k+1} \approx \omega_{i,j}^k + \mathcal{C}_{i,j}^k[\omega] + \mathcal{M}_{i,j}^k[\psi] + \mathcal{B}_{i,j}^k[T]. \tag{21}$$

$$T_{i,j}^{k+1} \approx T_{i,j}^k + \mathcal{D}_{i,j}^k[T] + \mathcal{J}_{i,j}^k[\psi]. \tag{22}$$

Here, $\mathcal{B}, \mathcal{C}, \mathcal{D}, \mathcal{J}, \mathcal{L}, \mathcal{M},$ and \mathcal{U} are the vectors of order $(p + 1) \times 1$ for each j . A code has been developed in MATLAB to find the numerical solutions of $\psi, \omega,$ and T at time $t = k + 1$. The computations have been started using the initial conditions and the iterations are repeated until the tolerance rate is achieved:

$$\left| \frac{\varpi^{k+1} - \varpi^k}{\varpi^k} \right| \leq 10^{-5}, \tag{23}$$

where ϖ represents a component of a general solution. Note that the considered numerical scheme is conditionally stable.

6. Results and discussion

The numerical findings for the convective heat transfer of a hybrid nanofluid in an inclined square cavity with a transverse magnetic field are provided and analyzed in this section. The governing factors for this study are nanoparticle volume fraction $\varphi,$ Rayleigh number $Ra,$ magnetic parameter $M,$ thermal radiation $Rd,$ and Eckert number $Ec.$ Table 2 illustrates the comparison of the Nusselt number with the results of previous studies.

In Fig. 2, typical streamlines and isotherms are illustrated for two different values of Rayleigh number $Ra = 10^3$ and $Ra = 10^4.$ The buoyancy-driven circulation flows within the cavity are noticeable due to the change in Rayleigh number and magnetic parameter. The magnitude of these circulations grows with the increasing Rayleigh number and lowers in the presence of the magnetic field. This is due to the buoyancy forces which grow stronger with Rayleigh number and overcome the viscosity forces. Moreover, the isotherms indicate that the average fluid temperature within the cavity rises, as does the flow obstruction caused by Lorentz force. The magnetic field creates drag-like forces known as the Lorentz force. These resistive forces, in turn, raise the temperature. As the magnetic parameter M increases, the Lorentz force grows. The fluctuations in the isotherms are more dominant for the higher value of $Ra.$ In Fig. 3, the isotherms and streamlines are illustrated for four different cases; (i) $Rd = 0$ and $M = 0,$ (ii) $Rd = 0,$ and $M = 10,$ (iii) $Rd = 2$ and $M = 0,$ and (iv) $Rd = 2$ and $M = 10.$ The results show that the amplitude of these flows is maximum in the absence of the magnetic field. It is also demonstrated that the radiation impacts are mostly felt on the streamlines in the center of the cavity, where the flow is least strong. The isotherms move away from the heated wall when a magnetic field is applied in either $Rd = 0$ or $Rd = 2.$ This is because of resistive Lorentz forces that are generated due to the magnetic field. The isotherm lines are curvier when $Rd = 0$ and $M = 0.$ Furthermore, the average fluid temperature increases when Rosseland’s heat flux is applied in horizontal and vertical directions, and the maximum temperature is observed in the presence of a magnetic field when $Rd = 2.$ The effects of Eckert number on the fluid flow and the temperature are depicted in Fig. 4. Eckert number is described as the kinetic energy to enthalpy driving force ratio in heat transfer. The findings show that the streamlines tend to move towards the center when the Eckert number increases, indicating that the viscous dissipation effects are dominating. The existence of viscous

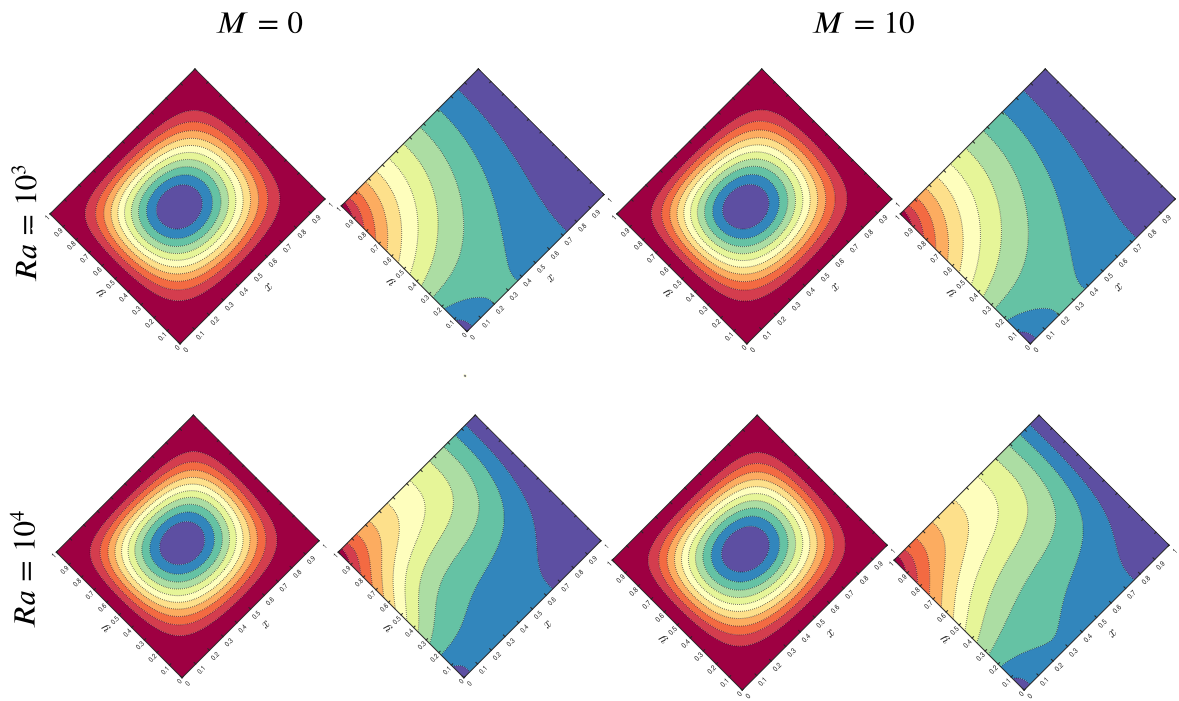


Fig. 2. Streamlines and isotherms against Ra .

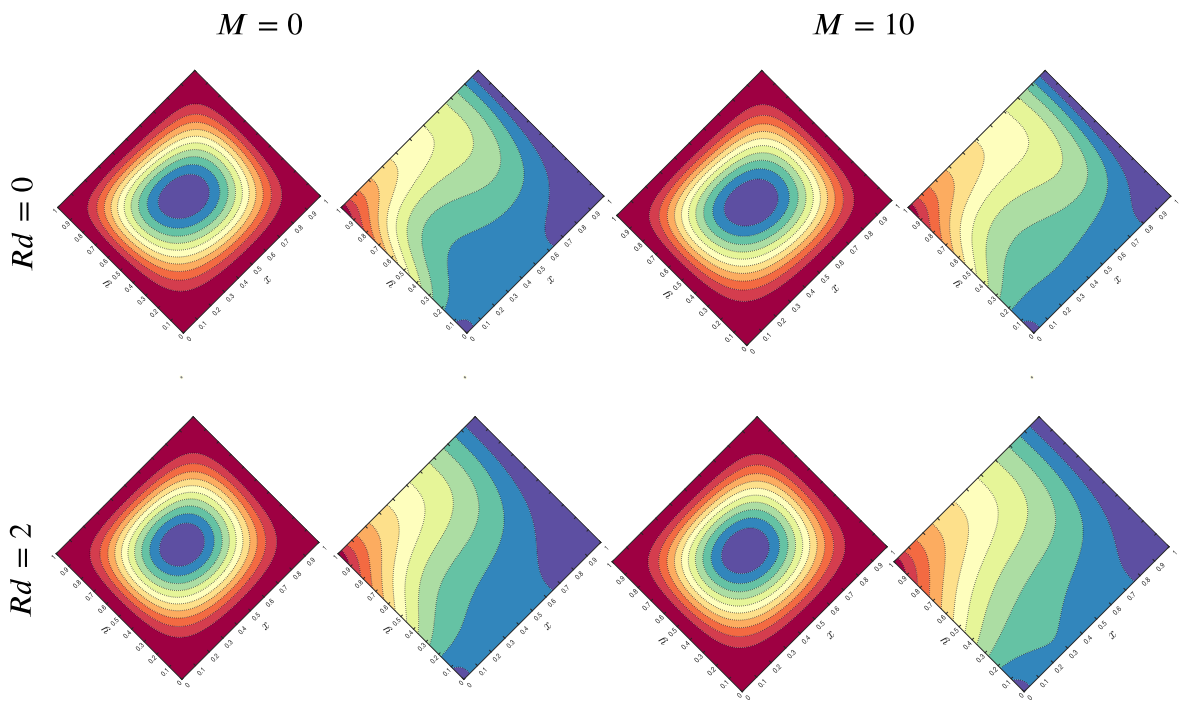


Fig. 3. Streamlines and isotherms against Rd .

Table 2
Comparison of Nu with previous studies.

Ra	Geridonmez and Oztop (2020)	Khanafer et al. (2003)	de Vahl Davis (1983)	Present
$Ra = 10^3$	1.118	1.118	1.118	1.1197
$Ra = 10^4$	2.246	2.245	2.243	2.4401
$Ra = 10^5$	4.518	4.522	4.519	4.5109
$Ra = 10^6$	8.810	8.826	8.799	8.8031

Table 3
Heat transfer rates of TiO₂/H₂O and Ag-TiO₂/H₂O with different values of ϕ and Ec .

ϕ	TiO ₂ /H ₂ O			Ag-TiO ₂ /H ₂ O		
	$Ec = 0.005$	$Ec = 0.008$	$Ec = 0.01$	$Ec = 0.005$	$Ec = 0.008$	$Ec = 0.01$
0	1.0889	0.98236	0.91186	1.0889	0.98236	0.91186
0.02	1.0924	0.98794	0.91896	1.0992	0.99283	0.92259
0.04	1.0952	0.99388	0.92673	1.1093	1.004	0.93416

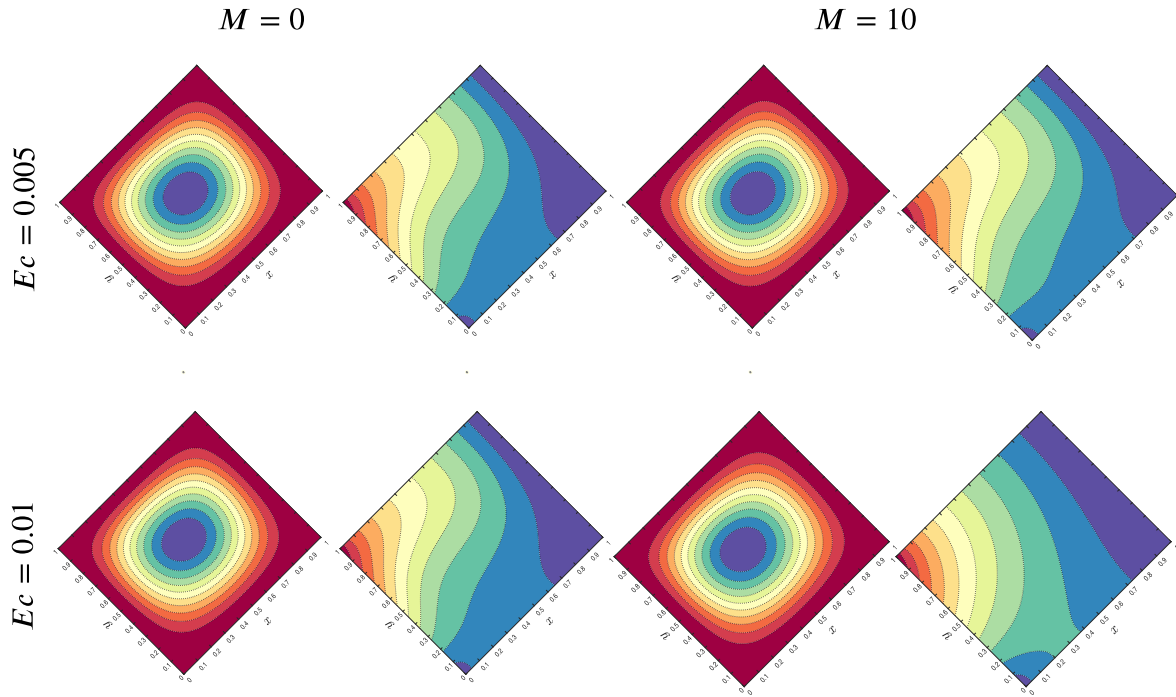


Fig. 4. Streamlines and isotherms against Ec .

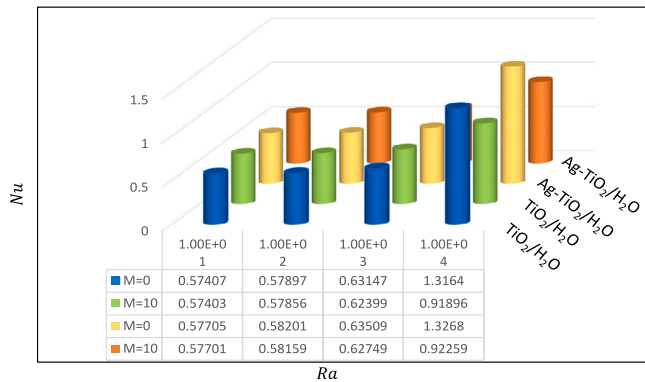


Fig. 5. Nusselt number against Ra .

dissipation has a substantial influence at the top-left and bottom-right corners with high flow velocities. Furthermore, the temperature rises when the Eckert number rises. The Eckert number is generated due to Joule heating, therefore, it does not have any effect When $M = 0$.

The consequences of Rayleigh number Ra on heat transfer rates of TiO₂/H₂O nanofluid and Ag-TiO₂/H₂O hybrid nanofluid are drawn in Fig. 5. Two different cases are considered: (i) without magnetic field ($M = 0$), and (ii) with magnetic field ($M = 10$). The results show that the heat transfer rates increased with the increasing values of Ra in both cases i.e., $M = 0$ and $M = 10$. Augmentation of Ra leads to increased circulation and convective energy transmission. There are

several ways in which increasing heat transfer rates might benefit the environment. For example, increasing the efficiency of a thermal system can aid in lowering energy usage. This can thus result in a reduced carbon footprint and a decrease in greenhouse gas emissions. In Fig. 6, the heat transfer rates of TiO₂/H₂O nanofluid and Ag-TiO₂/H₂O hybrid nanofluid are depicted for different values of Rd and M . It is found that the heat transfer rates are minimal when Rosseland's heat fluxes are applied to the system. Nusselt number decreases as the radiation parameter is increased because it modifies the isothermal lines (Fig. 3). However, maximum heat transfer rates are obtained when tiny Ag nanoparticles are added to TiO₂/H₂O. When $Rd = 0$, the heat transfer rates increased 0.5% on adding Ag nanoparticles to the fluid and the increment was 0.8% when thermal radiation was applied ($Rd = 2$).

In Table 3, the heat transfer rates are presented for different nanoparticle concentrations $\phi = 0\%, 2\%, 4\%$. It is evident from the results that the thermal efficiency of the cavity increases with increasing nanoparticle volume concentrations. This was expected since the thermal conductivity of nanoparticles is much higher than the thermal conductivity of a regular base fluid. As a result, increasing the concentration of nanoparticles in a base fluid eventually elevates the heat transfer rates. Here $\phi = 0$ corresponds to the regular base fluid which is pure water. Moreover, the effects of the Eckert number are also examined and it is found that the heat transfer rate decreases due to the viscous dissipation. However, maximum heat transfer rates are attained by the fluid with Ag-TiO₂/H₂O hybrid nanofluid compared to TiO₂/H₂O. The heat transfer of hybrid nanofluid is 2.5% and 0.8% greater compared to pure water and nanofluid, respectively. Table 4 illustrates the heat transfer rates for different cases of the magnetic field $M = 0, 5, 10$ for different fluids (i) pure water (ii) nanofluid,

Table 4
Heat transfer rates of H₂O, TiO₂/H₂O and Ag–TiO₂/H₂O with different values of *M* and *Ec*.

<i>M</i>	H ₂ O		TiO ₂ /H ₂ O		Ag–TiO ₂ /H ₂ O	
	<i>Ec</i> = 0.005	<i>Ec</i> = 0.01	<i>Ec</i> = 0.005	<i>Ec</i> = 0.01	<i>Ec</i> = 0.005	<i>Ec</i> = 0.01
0	1.315	1.315	1.3164	1.3164	1.3268	1.3268
5	1.1947	1.0987	1.1968	1.1027	1.2053	1.1094
10	1.0889	0.91186	1.0924	0.91896	1.0992	0.92259

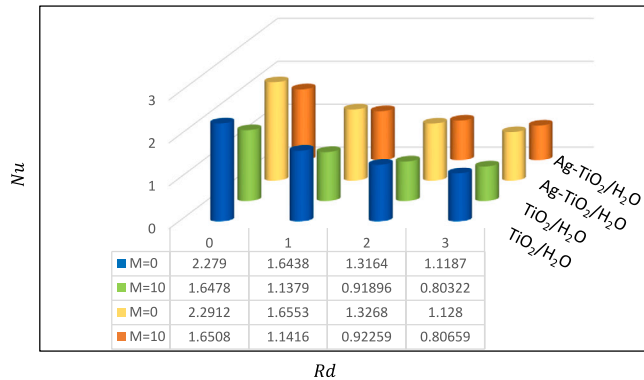


Fig. 6. Nusselt number against *Ra*.

and (iii) hybrid nanofluid. It is shown that the maximum heat transfer rates are obtained when magnetic effects are minimal. Likewise, heat transfer rates are decreased when Eckert number grows. However, these limitations can be overcome by adding tiny nanoparticles to the fluid. In the presence of the magnetic field, the heat transfer rates increased up to 0.8% and 1.2% on adding 2% vol. fraction of TiO₂ nanoparticles and Ag–TiO₂ hybrid nanoparticles in water-based fluid, respectively. When *M* = 0, the heat transfer increased up to 0.1% and 0.9% due to TiO₂ and Ag–TiO₂, respectively. These results showed that the effects of nanoparticles are more significant in the presence of a magnetic field.

7. Conclusions

This research aimed to minimize the energy consumption by increasing the thermal performance of a cavity using nanoparticles. In this regard, a hybrid nanofluid is prepared by adding tiny Ag and TiO₂ nanoparticles in water-based fluid. Meanwhile, the consequences of magnetic field, thermal radiation, and Joule heating are also examined. The 2D mathematical model was analyzed using a finite difference numerical approach. The key findings of the research are:

- The buoyancy-driven circulation flow within the cavity is noticeable due to the change in Rayleigh number and magnetic parameter.
- The fluid temperature is increased significantly when a magnetic field is applied in the presence of thermal radiation.
- The heat transfer rates increased up to 2.5% and 1.6% with 4% vol. of Ag–TiO₂ and TiO₂, respectively.
- The heat transfer capability of nanoparticles is enhanced when the magnetic field is applied.
- Addition of Ag in TiO₂/H₂O nanofluid increased the heat transfer rates by 0.2% without thermal radiation and 0.4% when the thermal radiation is applied.

The influence of the hybrid nanofluid can significantly increase the thermal performance of a cavity which is vitally important in solar thermal systems, heat exchangers, cooling/heating of buildings, thermal energy storage systems, geothermal systems, and food processing. There are several other ways in which the increasing heat transfer rates might benefit the environment. For example, increasing the efficiency of a thermal system can aid in lowering energy usage. This can thus

result in a reduced carbon footprint and greenhouse gas emissions. Besides the advantages, there are some limitations to adding nanoparticles in a base fluid. For example, the overall performance of the system may be hampered by the fluid’s stability and sedimentation.

CRedit authorship contribution statement

Hanifa Hanif: Writing – original draft, Software, Methodology, Investigation, Formal analysis, Conceptualization. **Sharidan Shafie:** Supervision, Resources. **Zainab Toyin Jagun:** Resources, Conceptualization.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data availability

No data was used for the research described in the article.

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